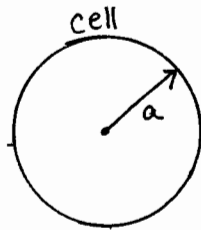


Problem 1

BE.430

Homework 1



Assumptions / Parameters:

- a) Steady state (S.S.)
- b) Zeroth-order consumption of O_2 in the cell, k_0
- c) $r = a$
- d) O_2 concentration c_1 just inside the cell, C_0 .
- e) consumption rate is spatially uniform

a) Conservation equation:

$$\frac{\partial c}{\partial t} = -\nabla \cdot N + R. \Rightarrow \frac{\partial c}{\partial t} \xrightarrow{0} = \frac{D}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial c}{\partial r} \right) - k_0 = 0$$

S.S.
↑
consumption

Boundary Conditions:

i) $c(r=r_0) = C_0$

ii) $\left. \frac{\partial c}{\partial r} \right|_{r=0} = 0$ due to spherical symmetry.

Solving:

$$\frac{D}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial c}{\partial r} \right) = k_0$$

$$\therefore c(r) = \frac{k_0 r^2}{6D} - \frac{C_1}{r} + C_2$$

$$\frac{\partial}{\partial r} \left(r^2 \frac{\partial c}{\partial r} \right) = \frac{k_0 r^2}{D}$$

General Equation

$$\int \partial \left(r^2 \frac{\partial c}{\partial r} \right) = \int \frac{k_0 r^2}{D} \partial r$$

$$r^2 \frac{\partial c}{\partial r} = \frac{k_0 r^3}{3D} + C_1$$

$$\frac{\partial c}{\partial r} = \frac{k_0 r}{3D} + \frac{C_1}{r^2}$$

$$\int \partial c = \int \left(\frac{k_0 r}{3D} + \frac{C_1}{r^2} \right) \partial r$$

Incorporate Boundary Conditions:

$$\frac{\partial c}{\partial r} = \frac{C_1}{r^2} + \frac{k_0 r}{3D} \Big|_{r=0} = 0 \quad \text{from ii)}$$

$$\therefore C_1 = 0$$

$$C(r=a) = \frac{k_0 a^2}{6D} + C_2 = C_0$$

$$\therefore C_2 = C_0 - \frac{k_0 a^2}{6D}$$

$$C(r) = C_0 + \frac{k_0}{6D} (r^2 - a^2)$$

$$\frac{D}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial c}{\partial r} \right) - k_0 = \frac{\partial c}{\partial t} \quad \cdot \text{Start with conservation equation.}$$

Scaling Factors: $t^* = \frac{1}{k_0}$, $c^* = C_0$, $r^* = a$

Nondimensionalize: $\tau = \frac{t}{t^*}$, $u = \frac{c}{c^*}$, $\rho = \frac{r}{r^*}$

$$\frac{C_0 D}{a^2 k_0} = 0.0036$$

↑ very small

∴ Diffusion limitation negligible

Substitute: $\frac{C_0 D}{a^2} \frac{\partial}{\partial \rho} \left(\rho^2 \frac{\partial u}{\partial \rho} \right) - k_0 = \frac{\partial u}{\partial \tau} \frac{C_0 k_0}{C_0 k_0}$

Damcholer # $\rightarrow \frac{C_0 D}{a^2 k_0} \frac{\partial}{\partial \rho} \left(\rho^2 \frac{\partial u}{\partial \rho} \right) - 1 = \frac{\partial u}{\partial \tau} C_0$

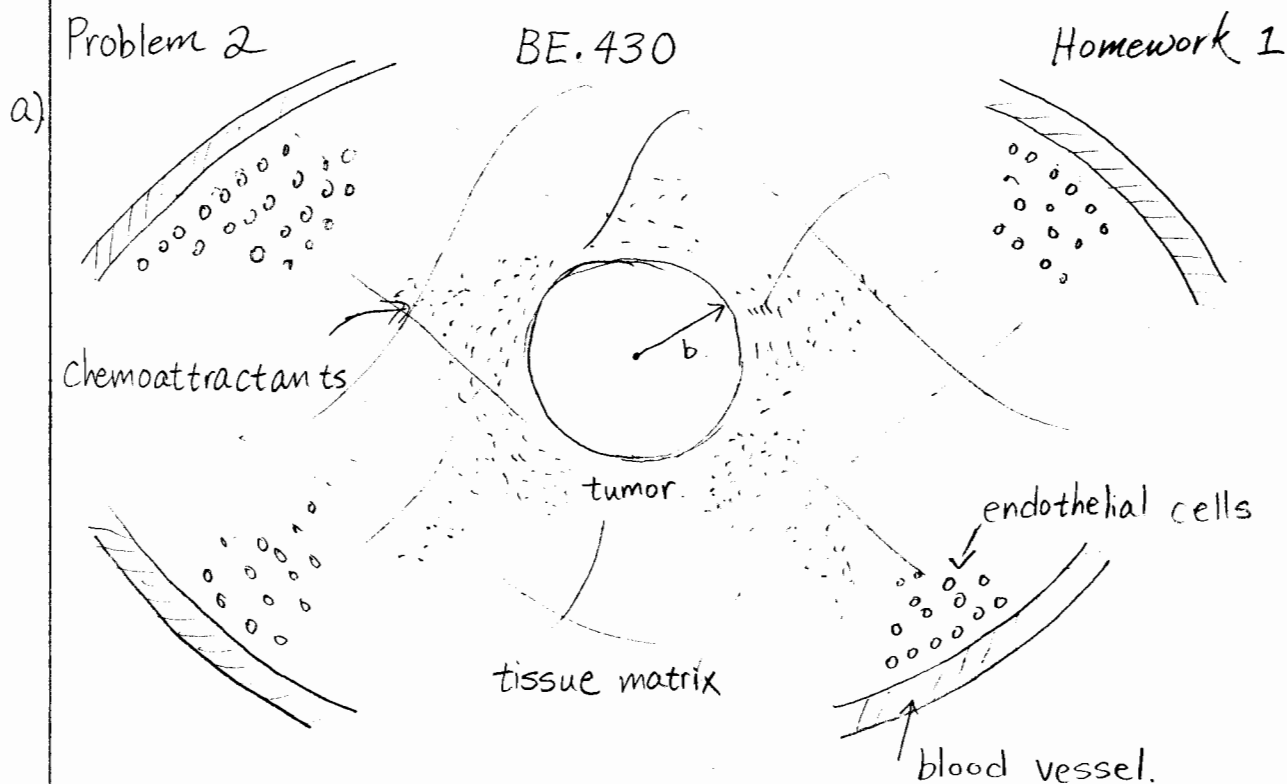
b) "Central core": $c(r=0) = 0$.

Assumption of zeroth order kinetics is no longer valid.

Find r_c such that $c(r=0) = 0$

$$C(r=0) = C_0 - \frac{k_0 r_c^2}{6D} = 0 \Rightarrow$$

$$r_c = \sqrt{\frac{6C_0 D}{k_0}}$$



Situation: tumor generates chemoattractants, which diffuse through the tissue matrix. Then, the endothelial cells on the blood vessel surface proliferate towards the tumor by perceiving a concentration gradient in the chemoattractants.

Assumptions:

- No reactive loss of chemoattractant
- Steady state
- spherical symmetry
- tissue is of infinite extent

Conservation Equation for tissue:

$$\frac{\partial c_c(r)^0}{\partial t} \underset{\text{s.s.}}{=} \frac{D}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial c}{\partial r} \right) + \underset{\substack{\uparrow \\ \text{no reactive loss}}}{R} \underset{>0}{}$$

Boundary conditions:

$$i) \text{ Flux Matching @ } r=b: \underbrace{-4\pi b^2 D}_{m^2} \underbrace{\frac{\partial C_c(r)}{\partial r}}_{\frac{\text{moles}}{m^2 \cdot s}} + \underbrace{R}_{\frac{\text{moles}}{s}} = 0$$

$$ii) \text{ Concentration @ } r=\infty: C(r=\infty)=0$$

Solve:

$$\frac{D}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial C}{\partial r} \right) = 0$$

$$\left(r^2 \frac{\partial C}{\partial r} \right) = B_1$$

$$\frac{\partial C}{\partial r} = \frac{B_1}{r^2}$$

$$\therefore C(r) = -\frac{B_1}{r} + B_2$$

$$C_c(r=\infty) = B_2 = 0 \quad \text{using B.C. i)}$$

$$\frac{\partial C_c(r)}{\partial r} = \frac{B_1}{r^2} \Big|_{r=b} = \frac{R}{4\pi b^2 D}$$

$$B_1 = \frac{R}{4\pi D} \quad \text{using B.C. ii)}$$

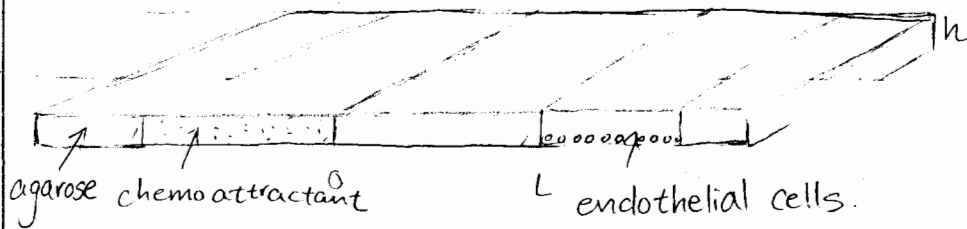
$$C_c(r) = -\frac{R}{4\pi D r}$$

$$= -\frac{1.983 \times 10^{-12}}{r}$$

$$\frac{\partial C_c(r)}{\partial r} = \frac{R}{4\pi D r^2}$$

$$= \frac{1.983 \times 10^{-12}}{r^2}$$

b)



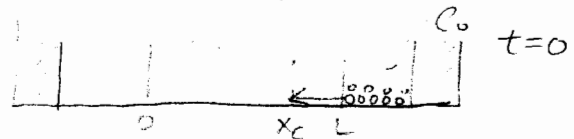
$$L \gg h$$

$$h \sim 1 \mu\text{m}$$

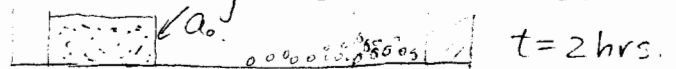
$$L \sim 1 \text{cm}$$

- Prepare a long, thin plate filled w/ agarose gel.
- Carve out two sections from the gel such for depositing chemoattractants and endothelial cells, respectively.
- At time $t=0$, place cells with concentration C_0 in well, mark them with trypan blue.
- At time $t=2\text{hrs}$, calculate D of cells, measuring distance that the cells have crawled in agarose gel, assuming cells diffuse slowly.

$$\therefore D(\text{cells}) = \frac{x_c^2}{2\text{hrs}} \quad \left(\frac{\text{cm}^2}{\text{s}} \right)$$



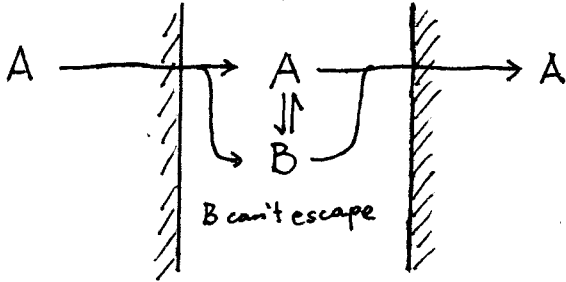
- At time $t=2\text{hrs}$, place attractants w/ concentration, a_0 , in well (marking them w/ fluorescent dye). Such that $a_0 \gg$ cells.



- C_0 is constant because cell diffusion is slow
- a_0 is constant because there's an abundance of attractants.

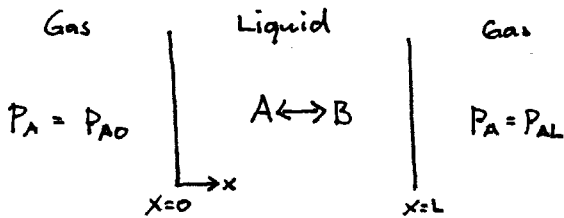
Assuming chemoattractants diffuse much faster than cells, we can assume quasi-steady state as soon as attractants are placed in the cell, thus inducing a linear concentration profile for the chemoattractants.

Problem 3 - Facilitated Transport

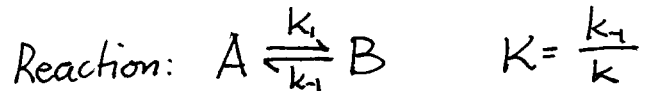


B is an alternative form of A.
 Ex. $A = \text{CO}_2$
 $B = \text{HCO}_3^-$
 (as in the respiratory system)

Schematic:



Solubility relation: $C_A = \alpha P_A$
 For simplicity, assume $D_A = D_B = D$



Assumptions:

1. Steady-state ($\frac{\partial}{\partial t} \rightarrow 0$)
2. 1-dimensional problem (liquid film of small thickness)
3. constant diffusivities ($D_A = D_B = D \neq f(c)$)
4. first-order reversible reaction
5. neglect convection, charge interactions, etc.

a) No reaction! Relate the flux of A to partial pressures and other system parameters

Species conservation of A: $\frac{\partial C_A}{\partial t} \xrightarrow{\text{st. st.}} = -\frac{\partial N_{x,A}}{\partial x} + R_A \xrightarrow{\text{no reaction}} = 0$

Constitutive equation (Fick's Law): $N_A = -D_A \frac{\partial C_A}{\partial x} = -D \frac{dC_A}{dx}$

$\Rightarrow D \frac{d^2 C_A}{dx^2} = 0$

Solving the ODE:

$$C_A(x) = Ax + B$$

Boundary conditions:

$$P(x=0^-) = P_{A0}$$

$$P(x=L^+) = P_{AL}$$

$$1. C(x=0^+) = \alpha P_{A0}$$

$$2. C(x=L^-) = \alpha P_{AL}$$

Applying B.C.s,

$$1. \alpha P_{A0} = A \cdot 0 + B$$

$$2. \alpha P_{AL} = A \cdot L + \alpha P_{A0}$$

$$\Rightarrow B = \alpha P_{A0}$$

$$\Rightarrow A = \frac{\alpha}{L} (P_{AL} - P_{A0})$$

$$\Rightarrow C_A(x) = \frac{\alpha}{L} (P_{AL} - P_{A0})x + \alpha P_{A0}$$

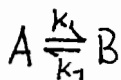
for no reaction case

(did not need to get here to solve part a)

Flux: $N_{x,A} = -D \frac{dc_A}{dx}$

$$N_{x,A} = -D \cdot \frac{\alpha}{L} (P_{AL} - P_{A0})$$

b) Determine the flux ^{of A} under reactive conditions.



with $K = \frac{k_1}{k_{-1}}$

Set up reaction kinetics:

$$A: \frac{\partial C_A}{\partial t} = -k_1 C_A + k_{-1} C_B = k_{-1} (K C_B - C_A) = R_A$$

$$B: \frac{\partial C_B}{\partial t} = -k_{-1} C_B + k_1 C_A = -k_{-1} (K C_B - C_A) = R_B = -R_A$$

Species conservation and constitutive equations:

$$A: \frac{\partial C_A}{\partial t} = D \frac{\partial^2 C_A}{\partial x^2} + R_A \quad (1)$$

$$B: \frac{\partial C_B}{\partial t} = D \frac{\partial^2 C_B}{\partial x^2} + R_B = D \frac{\partial^2 C_B}{\partial x^2} - R_A \quad (2)$$

Adding both equations:

$$D \frac{d^2 c_A}{dx^2} + D \frac{d^2 c_B}{dx^2} = 0 \Rightarrow \frac{d^2}{dx^2} (c_A + c_B) = 0 \quad (3)$$

Solve the ODE to obtain

$$c_A + c_B = A \frac{x}{L} + B \quad (4)$$

(We introduce the factor L to simplify things later)

Boundary conditions:

1. $c_A(x=0^+) = \alpha P_{A0}$

2. $c_A(x=L^-) = \kappa P_{AL}$

3. $\left. \frac{dc_B}{dx} \right|_{x=0^+} = 0$

4. $\left. \frac{dc_B}{dx} \right|_{x=L^-} = 0$

(no escape of B allowed \Rightarrow no flux condition)

Let's try to find another way to solve this problem.

Rearrange (4): $c_B = A \frac{x}{L} + B - c_A \quad (5)$

Insert (5) into (1): $D \frac{d^2 c_A}{dx^2} + k_1 (K(A \frac{x}{L} + B - c_A) - c_A) = 0$
 $\Rightarrow D \frac{d^2 c_A}{dx^2} + k_1 [K(A \frac{x}{L} + B) - (1+K)c_A] = 0$

Let $\eta = \frac{x}{L}$ for simplicity:

$$\frac{D}{L^2} \frac{d^2 c_A}{d\eta^2} + k_1 [K(A \cdot \eta + B) - (1+K)c_A] = 0$$

$$\Rightarrow \frac{d^2 c_A}{d\eta^2} + \frac{k_1 L^2}{D} [K(A \cdot \eta + B) - (1+K)c_A] = 0$$

Let $Da = \frac{k_1 L^2}{D}$ (this number will come up later in the semester)

$\lambda^2 = Da(1+K)$ (note that $Da(1+K)$ is always positive)

$$\Rightarrow \frac{d^2 c_A}{d\eta^2} - \lambda^2 c_A = -\frac{\lambda^2 K}{1+K} (A \cdot \eta + B) \quad (6)$$

This is a non-homogeneous second-order differential equation.

$$\text{Let } C_A(\eta) = C_A^{\text{homogeneous}}(\eta) + C_A^{\text{particular}}(\eta) \quad \text{where}$$

$C_A^{\text{homog.}}(\eta)$ is the solution to the homogeneous equation $\frac{d^2 C_A}{d\eta^2} - \lambda^2 C_A = 0$

Since λ^2 is always positive,

$$C_A(\eta) = C \sinh \lambda \eta + D \cosh \lambda \eta$$

The particular solution can be found by guessing: Let $C_A^{\text{part.}}(\eta) = C'(A\eta + B)$

Plug $C_A^{\text{part.}}(\eta)$ into (6)

$$\frac{d^2}{dx^2}(C'(A\eta + B)) - \lambda^2 C'(A\eta + B) = -\frac{\lambda^2 K}{1+K}(A\eta + B)$$

$$\Rightarrow C' = \frac{K}{1+K}$$

$$\Rightarrow C_A(\eta) = C \sinh \lambda \eta + D \cosh \lambda \eta + \frac{K}{1+K}(A\eta + B)$$

Recall boundary conditions (with $\eta = \frac{x}{L}$)

$$1. C_A(\eta=0) = \alpha P_{A0} \quad 3. \left. \frac{dC_B}{d\eta} \right|_{\eta=0} = 0$$

$$2. C_A(\eta=1) = \alpha P_{A1} \quad 4. \left. \frac{dC_B}{d\eta} \right|_{\eta=1} = 0$$

Applying B.C.s

$$1. \alpha P_{A0} = C \cdot \sinh \lambda \cdot 0 + D \cosh \lambda \cdot 0 + \frac{K}{1+K}(A \cdot 0 + B)$$

$$2. \alpha P_{A1} = C \cdot \sinh \lambda + D \cdot \cosh \lambda + \frac{K}{1+K}(A \cdot 1 + B)$$

From (4) (with $\eta = \frac{x}{L}$)

$$C_B = A \cdot \eta + B - C_A$$

$$= A \cdot \eta + B - C \sinh \lambda \eta - D \cosh \lambda \eta - \frac{K}{1+K}(A \cdot \eta + B)$$

$$= -C \sinh \lambda \eta - D \cosh \lambda \eta + \frac{1}{1+K}(A \cdot \eta + B)$$

$$\Rightarrow \frac{\partial C_B}{\partial \eta} = -C \cdot \lambda \cdot \cosh \lambda \eta - D \lambda \cdot \sinh \lambda \eta + \frac{1}{1+K} \cdot A$$

$$3. \quad 0 = -C \cdot \lambda \cosh \lambda \cdot 0 - D \lambda \sinh \lambda \cdot 0 + \frac{1}{1+K} A$$

$$4. \quad 0 = -C \cdot \lambda \cdot \cosh \lambda - D \lambda \sinh \lambda + \frac{1}{1+K} A$$

Rearranging:

$$\text{from 1.} \quad B = \frac{K+1}{K} (\alpha P_{A0} - D) \quad (a)$$

$$\text{from 3.} \quad A = (K+1) \lambda \cdot C \quad (b)$$

(b) into 4.

$$0 = -C \cdot \lambda \cdot \cosh \lambda - D \lambda \sinh \lambda + C \lambda$$

$$\Rightarrow C = \frac{D \sinh \lambda}{1 - \cosh \lambda} \quad (c)$$

$$\Rightarrow A = (K+1) \lambda \frac{D \sinh \lambda}{1 - \cosh \lambda} \quad (d)$$

2. and (a), (c), (d)

$$\alpha P_{AL} = \frac{D \sinh \lambda}{1 - \cosh \lambda} \sinh \lambda + D \cosh \lambda + \frac{K}{1+K} (K+1) \lambda^2 \frac{D \sinh \lambda}{1 - \cosh \lambda} + (\alpha P_{A0} - D)$$

$$\Rightarrow D = \frac{\alpha (P_{AL} - P_{A0}) (1 - \cosh \lambda)}{\sinh^2 \lambda + \cosh \lambda - \cosh^2 \lambda + K \lambda^2 \sinh \lambda - 1 + \cosh \lambda} \quad (\text{with } \sinh^2 \lambda - \cosh^2 \lambda = -1)$$

$$\Rightarrow D = \frac{\alpha (P_{AL} - P_{A0}) (1 - \cosh \lambda)}{2(\cosh \lambda - 1) + K \lambda \sinh \lambda}$$

$$C = \frac{\alpha (P_{AL} - P_{A0}) \sinh \lambda}{2(\cosh \lambda - 1) + K \lambda \sinh \lambda}$$

$$B = \frac{K+1}{K} \left(\alpha P_{A0} - \frac{\alpha (P_{AL} - P_{A0})}{2(\cosh \lambda - 1) + K \lambda \sinh \lambda} \right)$$

$$A = (K+1) \lambda \frac{\alpha (P_{AL} - P_{A0}) \sinh \lambda}{2(\cosh \lambda - 1) + K \lambda \sinh \lambda}$$

Determine the flux of c_A :

$$\frac{dc_A}{d\eta} = C\lambda \cos \lambda \eta + D\lambda \sinh \lambda \eta + \frac{K}{1+K} A$$

$$\Rightarrow N_A = -D^* \frac{dc_A}{d\eta} = -\frac{D^*}{L} (C\lambda \cos \lambda \eta + D\lambda \sinh \lambda \eta + \frac{K}{1+K} A)$$

$$\text{where } C = \frac{\alpha(P_{AL} - P_{A0}) \sinh \lambda}{2(\cosh \lambda - 1) + K\lambda \sinh \lambda} \quad D^* = \text{diffusivity}$$

$$D = \frac{\alpha(P_{AL} - P_{A0})(1 - \cosh \lambda)}{2(\cosh \lambda - 1) + K\lambda \sinh \lambda}$$

$$A = (K+1)\lambda \frac{\alpha(P_{AL} - P_{A0}) \sinh \lambda}{2(\cosh \lambda - 1) + K\lambda \sinh \lambda}$$

Btw. C and D terms are simplifyable.

c) Instead of simplifying the algebra to find a cleaner flux term, we recognize that the enhancement factor is only meaningful at the boundaries. We choose:

$$E = \frac{N_{x,A}|_{x=0} \text{ (with reaction)}}{N_{x,A} \text{ (w/o reaction)}}$$

We could obtain $N_{x,A}|_{x=0}$ from b); however, this requires tedious algebraic simplifications. So, we will recognize that from (3)

$$\frac{d^2}{dx^2} (C_A + C_B) = 0 \Rightarrow \frac{d}{dx} (C_A + C_B) = A$$

Since at the boundaries,

$$\left. \frac{dc_B}{dx} \right|_{x=0} = \left. \frac{dc_B}{dx} \right|_{x=L} = 0$$

$$\Rightarrow \left. \frac{dc_A}{dx} \right|_{x=0} = \left. \frac{dc_A}{dx} \right|_{x=L} = A$$

So,

$$N = -D \cdot (K+1) \lambda \frac{\alpha (P_{AL} - P_{A0}) \sinh \lambda}{2(\cosh \lambda - 1) + K \sinh \lambda}$$

$$\Rightarrow \boxed{E = \frac{(K+1) \lambda \sinh \lambda}{2(\cosh \lambda - 1) + K \sinh \lambda}}$$

For slow reactions, $\lambda \rightarrow 0$ ($k_1 \rightarrow 0$) with K fixed:

$$\sinh \lambda = \frac{e^\lambda - e^{-\lambda}}{2} \rightarrow \frac{(1 + \lambda + \dots) - (1 - \lambda + \dots)}{2} = \lambda + \dots$$

$$\cosh \lambda = \frac{e^\lambda + e^{-\lambda}}{2} \rightarrow \frac{(1 + \lambda + \frac{\lambda^2}{2}) + (1 - \lambda + \frac{\lambda^2}{2})}{2} = 1 + \frac{\lambda^2}{2}$$

$$\cosh \lambda - 1 \rightarrow \frac{\lambda^2}{2}$$

$$\Rightarrow \lim_{\lambda \rightarrow 0} E = \frac{(1+K) \lambda^2}{2(\frac{\lambda^2}{2}) + K \lambda^2} = 1 \quad \left(\text{i.e., no enhancement for} \right. \\ \left. \text{very slow reaction rate} \right)$$

For fast reactions, $\lambda \rightarrow \infty$ with K fixed:

$$\sinh \lambda \rightarrow \frac{e^\lambda}{2}$$

$$\cosh \lambda \rightarrow \frac{e^\lambda}{2}$$

$$\Rightarrow \lim_{\lambda \rightarrow \infty} E = \frac{(K+1) \lambda \frac{e^\lambda}{2}}{2\left(\frac{e^\lambda}{2} - 1\right) + K \lambda \frac{e^\lambda}{2}} \rightarrow \frac{K+1}{K}$$

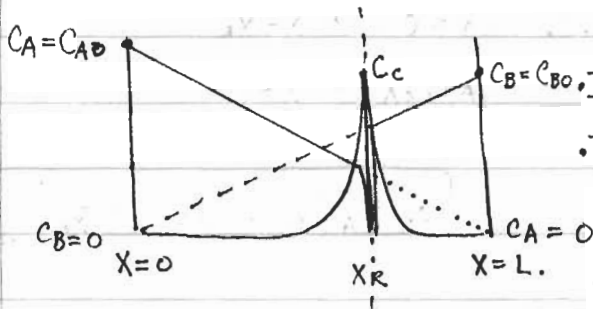
Thus, E is largest for $\lambda \gg 1$ (fast reaction) and $K \ll 1$.
At equilibrium ($R_{VA} = 0$),

$$\frac{C_B}{C_A} \Big|_{\text{eq.}} = \frac{1}{K}$$

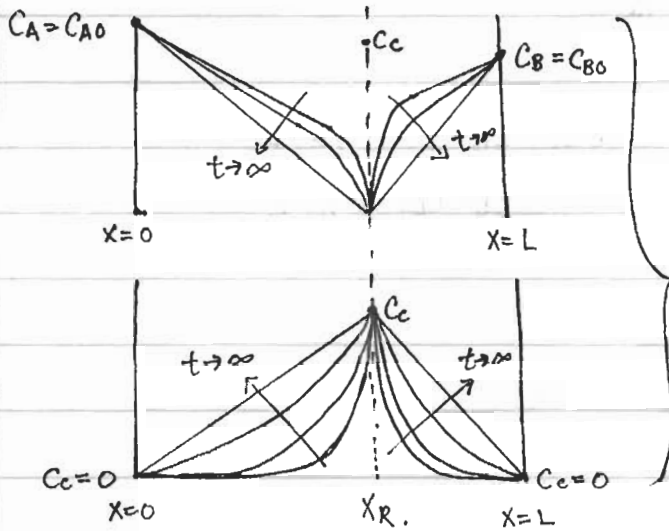
so that with $K \ll 1$, there is a lot of B present. This is what leads to the large flux enhancements.

Problem 4 (2.12 Deen) BE.430

Homework 1



Instant that $A+B \rightarrow C$, $t=t_0$
 • There's very fast reaction, $k \rightarrow \infty$
 $\therefore C_A = C_B = 0 @ x_R$
 • C_c spikes @ x_R



- As $t \rightarrow \infty$, the concentration profile becomes linear for all three species.
- Basically, if you assume s.s. before reaction, A & B both have a linear profile going from 0 to L & vice versa.

- Then, @ $t=t_0$, there's a sink for A & B @ $x=x_R$ where $C_A = C_B = 0$ immediately to form C, causing an impulse of C @ x_R .
- Eventually, depletion of A & B @ x_R forces A & B profiles to be linear again, a new s.s.
- Two boundary conditions @ $x=0, x=L$ for C_c also eventually force C_c to have linear profile on both sides. with $C_c(x_R^+) = C_c(x_R^-)$

Conservation of Species:

$$0 < x < x_R \quad \frac{\partial^2 C_A}{\partial x^2} + R_{AV} \overset{=0}{=} \frac{\partial C_A}{\partial t} \overset{=0}{=} \text{(steady state)}$$

↑
no reaction

$$x_R < x < x_L \quad \frac{\partial^2 C_B}{\partial x^2} + R_{BV} \overset{=0}{=} \frac{\partial C_B}{\partial t} \overset{=0}{=}$$

Assumptions:

- non homogeneous reaction $A+B \rightarrow C$ @ $x=x_R$.
- fast reaction @ $x=x_R$, $k \rightarrow \infty$
- steady-state
- dilute solution

Solve for $C_A(x)$, $C_B(x)$, X_R , $C_c(x)$

$$C_A: D_A \frac{\partial^2 C_A}{\partial x^2} = 0$$

$$\text{B.C. } C_A = 0 \text{ @ } x = X_R$$

$$C_A = C_{0A} \text{ @ } x = 0$$

$$C_A(x) = C_1 x + C_2$$

$$C_A(x=0) = C_2 = C_{0A}$$

$$\therefore C_A(x) = C_{0A} \left(1 - \frac{x}{X_R}\right)$$

$$C_A(x=X_R) = C_1 X_R + C_{0A} = 0$$

$$C_1 = -\frac{C_{0A}}{X_R}$$

$$C_B: D_B \frac{\partial^2 C_B}{\partial x^2} = 0$$

$$\text{BC: } C_B = 0 \text{ @ } x = X_R$$

$$C_B = C_{BL} \text{ @ } x = L$$

$$C_B(x) = C_3 x + C_4$$

$$C_B(x=X_R) = C_3 X_R + C_4 = 0$$

$$C_B(x=L) = C_3 L + C_4 = C_{BL}$$

$$C_3 (X_R - L) = -C_{BL}$$

$$C_3 = -\frac{C_{BL}}{X_R - L}$$

$$C_B(x) = -\frac{C_{BL}}{X_R - L} x + \frac{C_{BL} X_R}{X_R - L}$$

$$C_B(x) = C_{BL} \left(\frac{X_R - x}{X_R - L} \right)$$

X_R : • Use flux matching between C_A & C_B @ $x = X_R$

- If it's counter intuitive why there would be flux although $C_A = C_B = 0$ @ X_R @ S.S., remember the slope (flux) of the respective concentration profiles is NOT 0 @ $x = X_R$ and the heterogeneous reaction is shaping the concentration profile, not vice versa.

Problem 4 (2.12 Deen)

BE.430

Homework 1

$X_R: N_A = -N_B$

$$D_A \frac{\partial C_A}{\partial x} = -D_B \frac{\partial C_B}{\partial x}$$

$$D_A \left(\frac{-C_{0A}}{X_R} \right) = -D_B \left(\frac{-C_{BL}}{X_R - L} \right)$$

$$L - X_R = \frac{D_B}{D_A} \frac{C_{BL}}{C_{0A}} X_R$$

$$X_R = \frac{L}{1 + \frac{D_B C_{BL}}{D_A C_{0A}}}$$

Find the X_R such that the flux on both sides will match because you assume everything that comes to X_R reacts completely. in the forward

Boundary Conditions

$C_d: D_c \frac{\partial^2 C_c}{\partial x^2} = 0$ for $0 \leq x < X_R$
 $X_R \leq x \leq L$

a) $C_c^-(x=0) = C_c^+(x=L) = 0$

b) $C_c^+(x=X_R^+) = C_c^-(x=X_R^-)$

c) $-D_c \frac{\partial C_c^+}{\partial x}(x=X_R^+) + D_c \frac{\partial C_c^-}{\partial x}(x=X_R^-) = R_c$

Since there exists a 1:1:1 ratio in $A+B \rightarrow C$,

$-R_{SA} = -R_{SB} = R_{SC}$ (Note: $R_v = X C_A C_B$ given was not used)

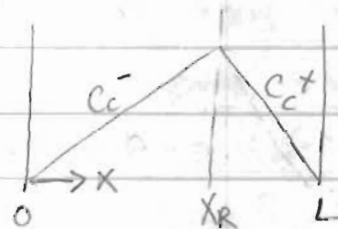
All @ surface

$N_A|_{x=X_R^+} - N_A|_{x=X_R^-} = R_{SA}$

$N_B|_{x=X_R^+} - N_B|_{x=X_R^-} = R_{SB}$

$N_C|_{x=X_R^+} - N_C|_{x=X_R^-} = R_{SC}$

Flux Matching @ X_R



$R_{SC} = \frac{D_A C_{0A}}{X_R} = -R_{SA}$

Solve:

$$C_c^-(x) = \alpha x + \beta$$

$$C_c^+(x) = \xi x + \theta$$

$$\textcircled{1} C_c^-(0) = \beta = 0 \quad \left. \vphantom{C_c^-(0)} \right\} \text{using B.C. a)}$$

$$\textcircled{2} C_c^+(x_L) = \xi x_L + \theta = 0$$

$$\textcircled{3} \alpha x_R = \xi x_R + \theta \quad \text{using B.C. b)}$$

$$\textcircled{4} -D_c \cdot \xi + D_c \alpha = \frac{D_A C_{0A}}{x_R} \quad \text{using B.C. c)}$$

$$\alpha = \frac{D_A C_{0A}}{D_c x_R} + \xi \quad \text{(i) from } \textcircled{4}$$

$$\theta = -x_L \xi \quad \text{(ii) from } \textcircled{2}$$

Substitute (i) & (ii) into $\textcircled{3}$

$$\frac{D_A C_{0A}}{D_c} + \xi x_R = \xi x_R - x_L \xi \Rightarrow \xi = -\frac{D_A C_{0A}}{D_c x_L};$$

$$\theta = \frac{D_A C_{0A}}{D_c}; \quad \alpha = -\frac{D_A C_{0A}}{D_c x_L} + \frac{D_A C_{0A}}{D_c x_R}$$

$$C_c(x) = \begin{cases} \frac{D_B C_{BL}}{D_c x_L} & 0 < x < x_R \\ -\frac{D_A C_{0A}}{D_c} \left(1 - \frac{x}{x_L}\right) & x_R < x < L \end{cases}$$