

Light with wavelengths  $< 290 \text{ nm}$  doesn't reach the earth's surface; this is UV light, and it's absorbed by ozone (see p. 161 figure). This means aniline will be effectively degraded by direct photolysis, since it absorbs light above  $290 \text{ nm}$ , but anilinium will not.

We want a pH where aniline predominates:

$$\frac{[C_6H_5NH_2][H^+]}{[C_6H_5NH_3^+]} = 10^{-4.6} \quad \text{at pH } 3.5, \frac{[An]}{[AnH^+]} = \frac{10^{-4.6}}{10^{-3.5}} = 0.079$$

$$\text{pH } 6.5, \frac{[An]}{[AnH^+]} = 79 \quad \text{pH } 9.5, \frac{[An]}{[AnH^+]} = 79,000$$

We would not want to acidify the water, because then anilinium would predominate. Raising the pH seems reasonable, but then an extra neutralizing step would be needed, which would add to the cost. At pH 6.5 there is still significantly more aniline (also, as aniline is degraded, more anilinium will get deprotonated to maintain equilibrium), so leaving the pH unchanged would be best.

i.  $K = 5 \times 10^{-3} \text{ cm/s}$

$$\frac{dh}{dx} = 0.02$$

$$n = 0.2$$

a) specific discharge

$$q_s = -K \frac{dh}{dx} = (5 \times 10^{-3} \text{ cm/s})(0.02) = \boxed{10^{-4} \text{ cm/s}}$$

(informal treatment of negative sign, which tells us flow is from higher head to lower head)

b) maximum velocity

$$v = \frac{q}{n} = \frac{10^{-4} \text{ cm/s}}{0.2} = \boxed{5 \times 10^{-4} \text{ cm/s}}$$

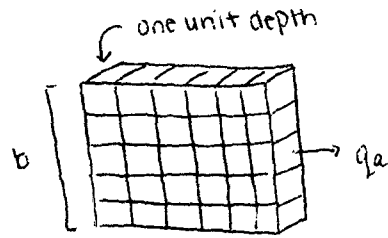
c)  $b = 5\text{ m}$

Transmissivity

$$T = kb = (5 \times 10^{-3} \text{ cm/s}) \times (500 \text{ cm}) = \boxed{2.5 \text{ cm}^2/\text{s}}$$

discharge per unit distance  $\perp$  to flow

$$bq = (500 \text{ cm}) \times (10^{-4} \text{ cm/s}) = \boxed{0.05 \text{ cm}^2/\text{s}}$$



$bq_e$  calculates discharge through a cross-sectional area of  $b \times 1$  unit

2.  $r_w = 0.1 \text{ m}$

$Q_w = 80 \text{ L/min}$

a) find drawdown  $\rightarrow$  this is steady-state, so use Theim equation

$$\begin{aligned}
 s_w &= \frac{Q_w}{2\pi kb} \ln\left(\frac{R}{r_w}\right) \\
 &= \frac{80 \text{ L/min}}{2\pi (5 \times 10^{-3} \text{ cm/s}) (5 \text{ m})} \ln\left(\frac{100 \text{ ft.}}{0.1 \text{ m}}\right) = \frac{0.38 \text{ m}^3/\text{min}}{2\pi (0.003 \text{ m/min}) (5 \text{ m})} \ln\left(\frac{30.48 \text{ m}}{0.1 \text{ m}}\right) \\
 &= \boxed{4.9 \text{ m}}
 \end{aligned}$$

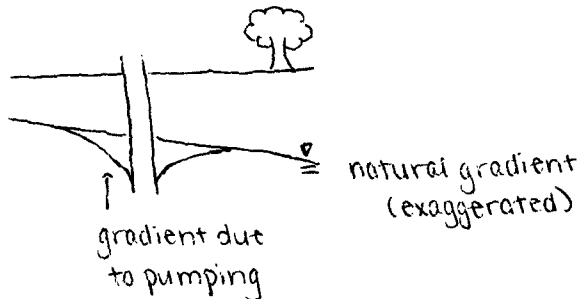
b) find hydraulic gradient due to the well:

$$\frac{ds}{dr} = \frac{Q_w}{2\pi kbr} = \frac{0.849 \text{ m}}{r}$$

at 20 ft.  $\frac{ds}{dr} = \frac{0.849 \text{ m}}{20 \text{ ft.}} \times \frac{1 \text{ ft.}}{.3048 \text{ m}} = 0.139$

at 75 ft.  $\frac{ds}{dr} = \frac{0.849 \text{ m}}{75 \text{ ft.}} \times \frac{1 \text{ ft.}}{.3048 \text{ m}} = 0.037$

This gradient, which is "downhill" towards the well in all directions, can be superimposed on the natural gradient.



upstream:



pumping-induced gradient enhances natural gradient

$$20 \text{ ft: } \frac{dh}{dx} + \frac{ds}{dr} = 0.02 + 0.139 = 0.159$$

$$75 \text{ ft: } 0.02 + 0.037 = 0.057$$

downstream:

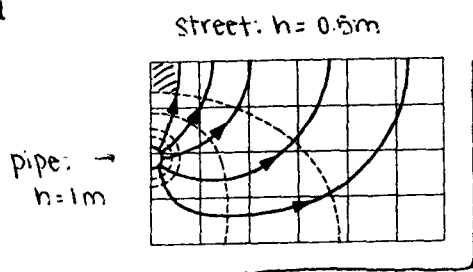


pumping-induced gradient counteracts natural gradient

$$20 \text{ ft: } \frac{dh}{dx} - \frac{ds}{dr} = 0.02 - 0.139 = -0.119$$

$$75 \text{ ft: } 0.02 - 0.037 = -0.017$$

7.



clayey soil  
(very low  $k$ )  $\Rightarrow$   
no-flow boundary

$$k = 10^{-3} \text{ cm/sec}$$

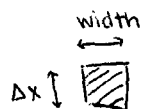
Also note that we are only given  
half the flow net (i.e. 12 streamtubes  
total).

find  $q$  per meter of pipe:

1) find discharge in one square (top left corner)

$$\Delta h = \frac{1\text{m} - 0.5\text{m}}{5} = 0.1\text{m}$$

$$\Delta x = 0.3\text{m}$$



$$q = -k \frac{dh}{dx} = 10^{-3} \text{ cm/s} \times \frac{0.1\text{m}}{0.3\text{m}} = 3.3 \times 10^{-4} \text{ cm/s}$$

2) find discharge (flow) through this streamtube



Cross-sectional area ( $\perp$  to  $q_a$ ) =  
width of square  $\times$  1m

$\perp$  because we want  $Q$  "per meter of pipe"

$$Q = q A = 3.3 \times 10^{-4} \text{ cm/s} (0.3\text{m})(1\text{m})$$

$$= 1 \text{ cm}^3/\text{s}$$

3) for total discharge, multiply by # of streamtubes (because there is an equal amount of discharge in each streamtube)

$$Q_{\text{tot}} = 1 \text{ cm}^3/\text{s} \times 12 = \boxed{12 \text{ cm}^3/\text{s}} \quad (\text{per m of pipe})$$

The flow net is not very accurate because the aspect ratio is not constant - some blocks are like squares, while others are like rectangles.

Alternative calculation (but you should understand the first one!):

$H = 0.5 \text{ m}$  total head drop

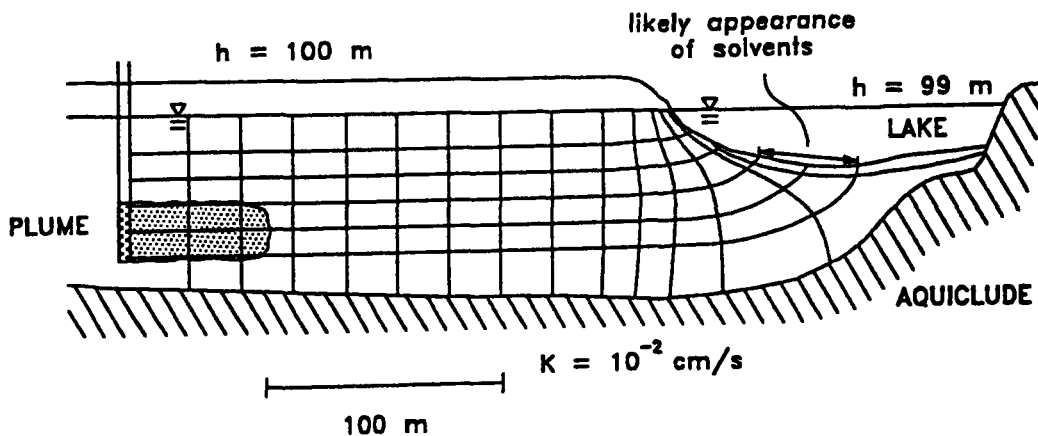
$n_d = 5$  # head drops

$n_f = 12$  # streamtubes

$$Q_f = \frac{n_f}{n_d} k \cdot H = \frac{12}{5} (10^{-3} \text{ cm/s}) (50 \text{ cm}) = 0.12 \text{ cm}^2/\text{s} \times 100 \text{ cm} = 12 \text{ cm}^3/\text{s}$$

↑  
1 m of pipe

9.



-- Flow doesn't cross streamlines (note that we are neglecting diffusion + dispersion), so the solvents will appear at the lake bed wherever the appropriate streamtubes end up.

distance  $\approx 300 \text{ m}$

$$q = -k \frac{dh}{dx} = 10^{-2} \text{ cm/s} \times \frac{1 \text{ m}}{300 \text{ m}} = 3.3 \times 10^{-5} \text{ cm/s}$$

$$v = \frac{q}{n} = \frac{3.3 \times 10^{-5} \text{ cm/s}}{0.3} = 1.1 \times 10^{-4} \text{ cm/s}$$

-- assume a value of  $n$   
(0.2 to 0.4, p. 208)

$$t = \frac{\text{distance}}{\text{velocity}} = \frac{300 \text{ m}}{1.1 \times 10^{-4} \text{ cm/s}} \times \frac{100 \text{ cm}}{\text{m}} = 2.7 \times 10^8 \text{ sec}$$

$$2.7 \times 10^8 \text{ s} \times \frac{\text{day}}{86,400 \text{ s}} \times \frac{\text{yr}}{365 \text{ d}} = 8.6 \text{ years} \approx \boxed{9 \text{ years}}$$

this is a rough approximation!

To be more precise, we could calculate the travel time across each square (if this level of precision is necessary), as done in Example 3-2.